BINDURA UNIVERSITY OF SCIENCE EDUCATION

FACULTY OF SCIENCE AND ENGINEERING

AEH 308

Department Of Engineering and Physics Bachelor of Science (Honours) in Agricultural Engineering Food Engineering

3 HOURS (100 MARKS)

INSTRUCTIONS

= JUN 2024

Answer any FOUR questions. Each question carries 25 marks.

Question 1

a. Use a Pearson Square to calculate the amounts of orange juice (10% sugar content) and sugar syrup (60% sugar content) needed to produce 50 kg of fruit squash containing 15% sugar. [5 marks]

b. Peas which have an average diameter of 6 mm and a density of 880 kgm⁻³ are dried in a fluidised-bed drier. The minimum voidage is 0.4 and the cross-sectional area of the bed is 0.25m². Calculate the minimum air velocity needed to fluidise the bed if the air density is 0.96 kg m⁻³ and the air viscosity is 2.15 x 10⁻⁵ N s m⁻². [5 marks]

c. Calculate the component mass balance for mixing ingredients to make 25 kg of beef sausages having a fat content of 30%, using fresh beef meat and beef fat. Typically, beef meat contains 18% protein, 12% fat and 68% water and beef fat contains 78% fat, 12% water and 5% protein.

[5 marks]

d. Briefly explain five factors that affect the duration of completely frying foods.

[10 marks]

Question 2

a. Highlight five main advantages of fermentation as a method of food processing.

[5 marks]

b. Briefly explain four factors that affect the rate of food separation through a screen.

[8 marks]

c. Brewers' yeast is grown continuously in a fermenter with an operating volume of 12 m³. The residence time is 20 h and the yeast has a doubling time of 3.2 h. If a 2% inoculum, which contains 5% yeast cells is mixed with the substrate, calculate the mass of yeast harvested from the fermenter per hour. It is given that the density of broth is 1010 kgm⁻³.

[12 marks]

Question 3

a. Milk containing 3.7% fat and 12.8% total solids is to be evaporated to a produce a product containing 7.9% fat. Assuming that there are no losses during the process, calculate:

i. the yield of product from 100 kg of milk and

[5 marks]

ii. the total solids concentration in the final product.

[5 marks]

b. Briefly describe five methods of peeling fruits and vegetables.

[15 marks]

Question 4

- a. Corn meal with a moisture content of 18% (wb) is being extruded through a metering zone of an extruder with the following dimensions of the channel: width 8 cm, height 3 cm, length 65 cm. The wall velocity is estimated to be 0.35 m/s. The rheological properties of the extrudate can be estimated by a viscosity of 66,700 Pa s and a density of 1980 kg/m³. If the pressure drop is maintained at 3500 kPa, calculate the mass flow rate of extrudate through the die. [5 marks]
- b. Explain four factors that affect the degree of mixing solid food particles. [8 marks]
- c. Calculate the size of the motor required to blend olive oil and rape-seed oil in a ratio of 1 to 5 by a propeller agitator 20 cm in diameter operating at 750 rpm in a cylindrical tank of 1 m diameter at 20°C. It is given that Po is 0.5, the viscosity of olive oil at 20°C is 0.084 Nsm⁻², the density of olive oil 910 kg m⁻³, the viscosity of rape-seed oil 0.118 Nsm⁻² and the density of rapeseed oil 900 kg m⁻³.

[12 marks]

Question 5

a. Highlight two advantages of ohmic heating as compared to microwave heating.

[2 marks]

b. An 8 kW oven has a hearth area of 4 m² and operates at 210°C. It is loaded with two batches of bread dough in baking tins; 150 loaves on the first batch and 120 loaves on the second batch. The surface of each loaf measures 12 cm x 20 cm. Assuming that the emissivity of dough is 0.85, that the dough bakes at 100°C, and that 90% of the heat is transmitted in the form of radiant energy, calculate the efficiency of energy use for each batch.

[10 marks]

c. Beer with a specific gravity of 1.042 and a viscosity of 1.40 x10⁻³N s m⁻² contains 1.5% solids which have a density of 1160 kg m⁻³. It is clarified at the rate of 240 l h⁻¹ in a bowl centrifuge which has an operating volume of 0.09 m³ and a speed of 10 000rpm. The bowl has a diameter of 5.5 cm and is fitted with a 4 cm outlet. If the bowl speed is increased to 15 000 rpm, calculate:

i. the new feed rate, and

[7 marks]

ii. minimum rev particle size that can be removed at the new speed.

[6 marks]

Question 6

a. Explain four factors that influence the rate of heat transfer when freezing foodstuffs.

[8 marks]

b. Pulp which contains 15% solids is filtered in a plate and frame fitter press with a pressure difference of 290 Pa and a 5.5 m² filter area. The masses of filtrate are shown below for a 1.5 h cycle.

of fittings and shorting sector, i.e. a river a just						
Time (min)	7.5	30.4	50	90		
Mass of filtrate (kg)	1800	3800	4900	6800		

If the cake is incompressible and the viscosity of the filtrate is $1.33 \times 10^{-3} \text{Nsm}^{-2}$, calculate:

i. the specific resistance of the cake, and

[10 marks]

ii. the volume of filtrate that would be obtained if the cycle time were reduced to 45 min.

[7 marks]

End of paper

FOOD ENGINEERING (AEH308)

MATHEMATICAL FORMULAE

GRINDING AND CUTTING

$$dE/dL = KL^n$$

Kick

 $K = K_{\rm K} f_{\rm c}$

 $\mathrm{d}E/\mathrm{d}L = K_{\mathrm{K}}f_{\mathrm{c}}L^{-1}$

 $E = K_{\rm K} f_{\rm c} \log_{\rm e}(L_1/L_2)$

[law]

Rittinger

 $K = K_{\rm R} f_{\rm c}$

 $dE/dL = K_R f_c L^{-2}$

 $E = K_{\rm R} f_{\rm c} (1/L_2 - 1/L_1)$

[law]

Bond

 $E = E_i (100/L_2)^{1/2} [1 - (1/q^{1/2})]$

[law]

 $q = L_1/L_2$

Modification of the grinding energy equations

Energy required E (kWh/kg) for reducing particle size from x_1 to x_2

Rittinger

$$E = K_R \left(\frac{1}{x_2} - \frac{1}{x_1} \right)$$

Kick

$$E = K_k \ln \left(\frac{x_1}{x_2} \right)$$

Bond

$$E = K_B \left[\left(\frac{1}{x_2} \right)^{\frac{1}{2}} - \left(\frac{1}{x_1} \right)^{\frac{1}{2}} \right]$$

EXTRACTION / LEACHING WASHING

$$\alpha = \frac{Ce}{Cr}$$

 $\Phi vfCf + \Phi vsCs = \Phi veCe + \Phi vrCr$

 $\frac{\text{Amount extracted}}{\text{Amount in raffinate}} = \frac{\phi \text{veCe}}{\phi \text{vrCr}} = \alpha \frac{\phi \text{ve}}{\phi \text{vr}} = S$

NB// for single stage

$$S = \frac{Vs}{Vr}$$

Non extracted fraction = $1 - f = \frac{Cr}{Cf} = \frac{1}{1 + S}$

Where f=extracted fraction

$$f = \frac{\text{amount extracted}}{\text{amount in feed}} = \frac{\phi \text{veCe}}{\phi \text{vfCf}}$$

Therefore for only 1 stage, $f = \frac{S}{S+1}$

For multistage:

$$N = \frac{\ln\left[\left(\frac{S-1}{1-f}\right)+1\right]}{\ln S} - 1$$

REFRIGERATION CHILLING AND FREEZING

Plank's equation

$$t_f = \left\lceil \frac{\left(\rho \Delta H_L\right)}{\left(T_f - T_a\right)} \right\rceil \left[\left(\frac{2 \operatorname{Pr}}{h}\right) + \left(\frac{4 R r^2}{\lambda}\right) \right]$$

 ΔH_L = the latent heat of crystallisation of ice (334kJ/kg)

Shape factors

		Shape			
	Sphere	Infinite Plate	Infinite Cylinder		
Shape factor	P=1/6, R=1/24	P=1/16, R=1/24	P=1/16, R=1/24		

Pham's equation

$$t_f = \frac{1}{E} \left[\left(\frac{\Delta H_1}{\Delta T_1} \right) + \left(\frac{\Delta H_2}{\Delta T_2} \right) \right] \left[\left(\frac{r}{h} \right) + \left(\frac{r^2}{2\lambda} \right) \right]$$
$$\Delta T_1 = 0.5 (T_1 + T_{\text{fm}}) - T_a$$

 $\begin{array}{l} \Delta T_2 = T_{\text{fin}} - T_a \\ \Delta H_1 = \rho C_{\text{pu}} (T_i - T_{\text{fin}}) \end{array}$

 $\Delta H_2 = \rho \Delta H_L + \rho C_{pf} (T_{fin} - T_{fin})$ $T_{fin} = 1.8 + 0.263 T_{fin} + 0.105 T_{e}$

$$E = 1 + \left[\frac{\left(1 + \left(\frac{2}{\beta_{i}}\right)\right)}{\left(\beta_{1}^{2} + \left(\frac{2\beta_{1}}{\beta_{i}}\right)\right)} + \left(\frac{\left(1 + \left(\frac{2}{\beta_{1}}\right)\right)}{\beta_{2}^{2} + \left(\frac{2\beta_{2}}{\beta_{i}}\right)}\right)\right]$$

The shape $\beta_1 = A/(\pi r^2)$ $B_2 = 3V/(4\pi\beta_1 r^3)$ $B_i = (\ln r)/\lambda$, Biot number

SEDIMENTATION

$$u = \frac{\left[d_{st}^2(\rho_s - \rho)g\right]}{18\mu}$$

FILTRATION

$$\frac{\delta V}{\delta t} = \frac{\left(A\Delta P\right)}{R}$$

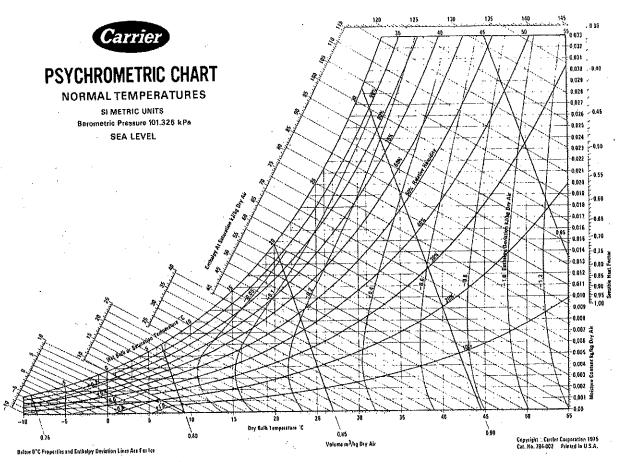
$$R = \mu w(L_c + L)$$

$$L_c = \frac{wV}{A}$$

$$R = \mu t r \left[w \left(\frac{V}{A} \right) + L \right]$$

$$\frac{\delta V}{\delta t} = \frac{A\Delta P}{\mu tr[w(\frac{V}{A}) + L]}$$

$$\Delta P = \frac{V}{At} \times \mu tr \left[vv \left(\frac{V}{A} \right) + L \right]$$



Reproduced courtesy of Carrier Corporation

++++